

Using Membrane Pervaporation for the Dehydration and Degassing of Solvents for Reuse in Chemical Manufacturing

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June 25, 2018
Hannah Murnen

In a nutshell

Membrane pervaporation for dehydration of organic solvents is important across a number of industries, including pharmaceutical manufacturing (focus of this talk)

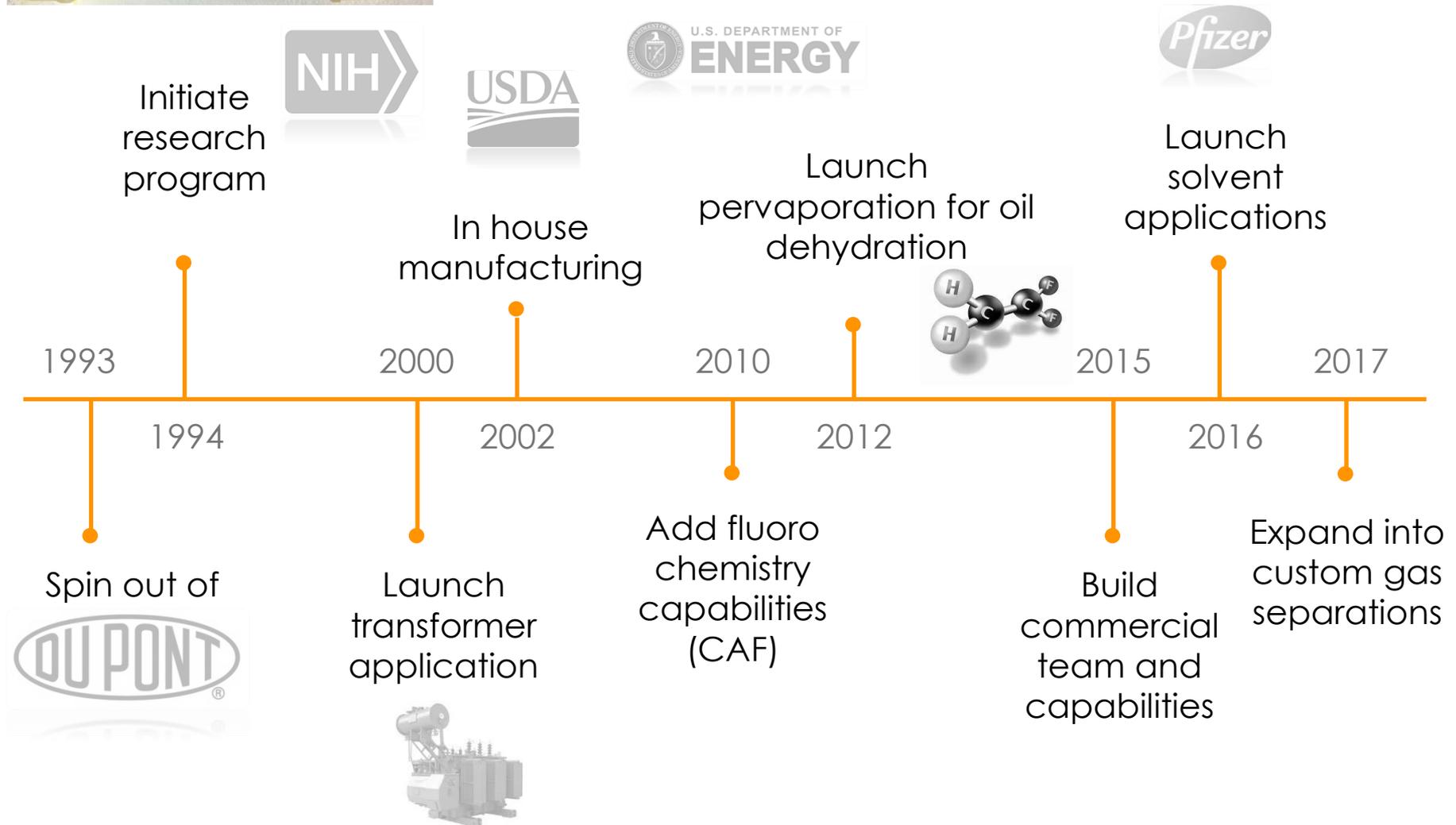
Perfluoropolymer membranes are an ideal system for solvent dehydration given their high chemical resistance and high flux and selectivity

Design of these systems is intricate and requires a careful analysis of membrane, system and application requirements

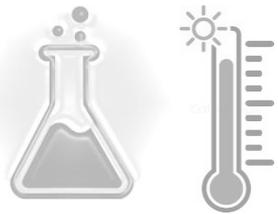
An example of a pharmaceutical system, designed in collaboration with Pfizer, will be used to demonstrate important design concepts and the eventual implementation of a successful system

Introduction to Compact Membrane Systems

Compact Membrane Systems



CMS is a technology player with platform and applications across multiple industries



High chemical and thermal resistance

Fluoropolymer chemistry expertise and know how

Industry application understanding

Petrochem
Pharma
Oil and Gas
Manufacturing
Wind Power
Marine
Power Gen
Aerospace
Chemicals

Membrane, prototype, manufacture, system design

IP in materials and applications

Effective in challenging environments where other materials fail

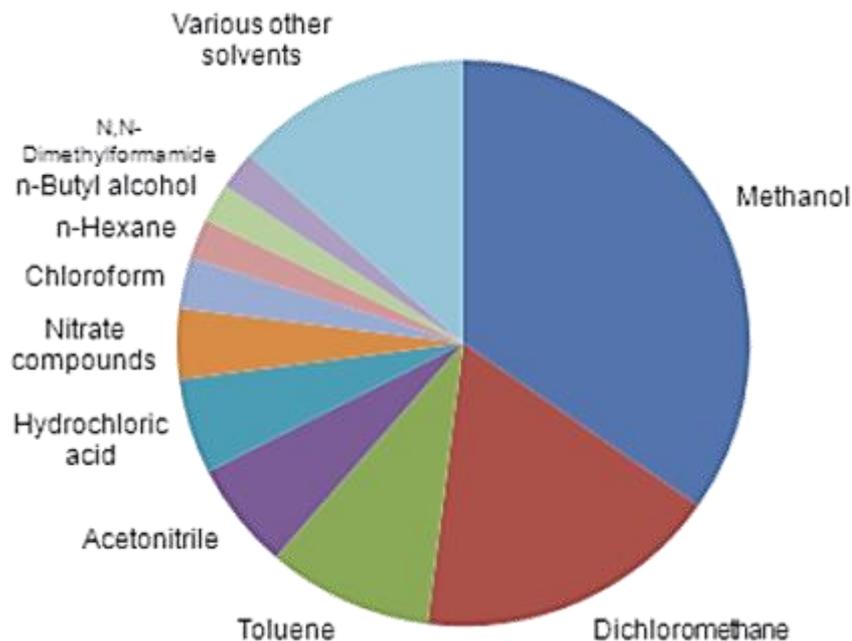
Applications in process chemistries and aggressive end products

Remove gases and water from organics

Why is solvent dehydration important in pharmaceutical production?

Solvent recovery and reuse is a big issue for API production

Total pharmaceutical use in 2006 of 128 MM Kg



Solvent purity can impact yield and efficacy of reaction, particularly in flow processes

- API production often requires use of organic solvents
- Typical solvent use is 10-800 kg/kg of API
- Accounts for up to 60% of raw materials usage -
- Solvent use is expensive (purchase, use, disposal)

¹Jimenez-Gonzalez, C., et al., Inter. J. Life Cycle Assessment 2004, 9(2), 114-121.

²Slater, C.S.; Savelski, M.J.; Hesketh, R.P. Abstracts of Papers, American Chemical Society 10th Green Chem. Eng. Conf., Washington DC, June 2006, American Chemical Society, 10.

³EPA TRI 2016, Pharmaceutical Industry

Continuous processing is the way of the future

Feature

Continuing Progress in Continuous Manufacturing

Process design, measurement, and control for enabling continuous processing adoption in pharmaceutical manufacturing.

By Doug Hausner, Jonathan Lustri, and Paul Brodbeck

The shift from batch to continuous production methods is transforming the future of pharmaceutical manufacturing. The potential economic gains from increasing capacity utilization and reducing the length of process development, product release times, and capital costs are driving the paradigm shift. Spurred by potential improvements to quality, patient safety, and the time required for breakthrough medicines to reach patients, even the U.S. Food and Drug Administration (FDA) has advocated a move to continuous manufacturing (CM).¹ However, with new methods come new challenges—particularly for process design, measurement, material traceability, and control.

Drivers for Continuous Manufacturing

The economic benefits of continuous methods over batch exist in nearly all areas of manufacturing and are the primary reason most industries have used continuous methods for decades. The FDA and other agencies have recently made it clear that they will not only accept CM, but that they support it as an enabler for true Quality by Design (QbD). In the case of secondary solid dosage, CM allows for much

Manufacturers, suppliers, and research institutions are collaborating to solve these challenges at projects across the globe, including the Engineering Research Center for Structured Organic Particulate Systems (CSOPS), based at Rutgers, the State University of New Jersey. This article provides a summary of the status of continuous processing in the pharmaceutical industry and considerations—based in part on research at CSOPS—for how manufacturers can overcome the challenges related to quality, compliance, material traceability, and process design and control.




Pharmaceutical Manufacturing in the 21st Century-From Batch to Continuous Manufacturing-An FDA Perspective

presented by **Dr Sau (Larry) Lee**
followed by **Dirk Leister**

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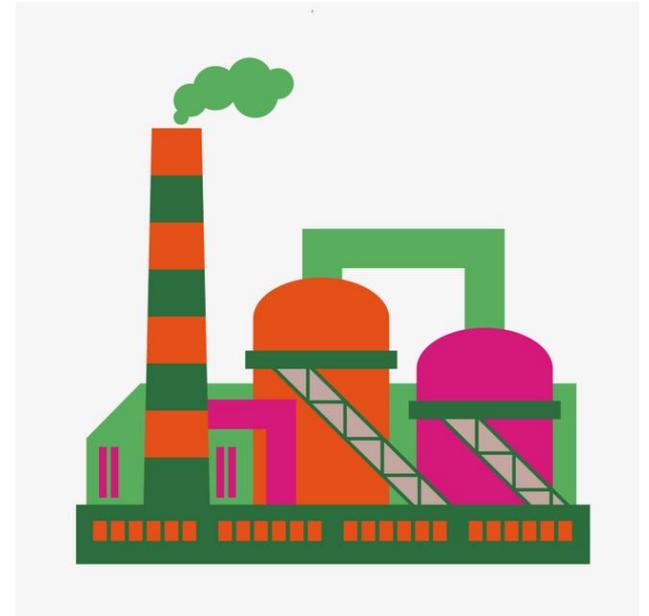
BioPharma
Asia

CONTINUOUS REVOLUTION

AT THE **NOVARTIS-MIT CENTER FOR CONTINUOUS MANUFACTURING**, SCIENTISTS ARE USING LEAN ENGINEERING PRINCIPLES AND SOPHISTICATED TECHNOLOGY TO MAKE A QUANTUM LEAP FORWARD IN THE WAY MEDICINES ARE MANUFACTURED

Where else could solvent dehydration be useful?

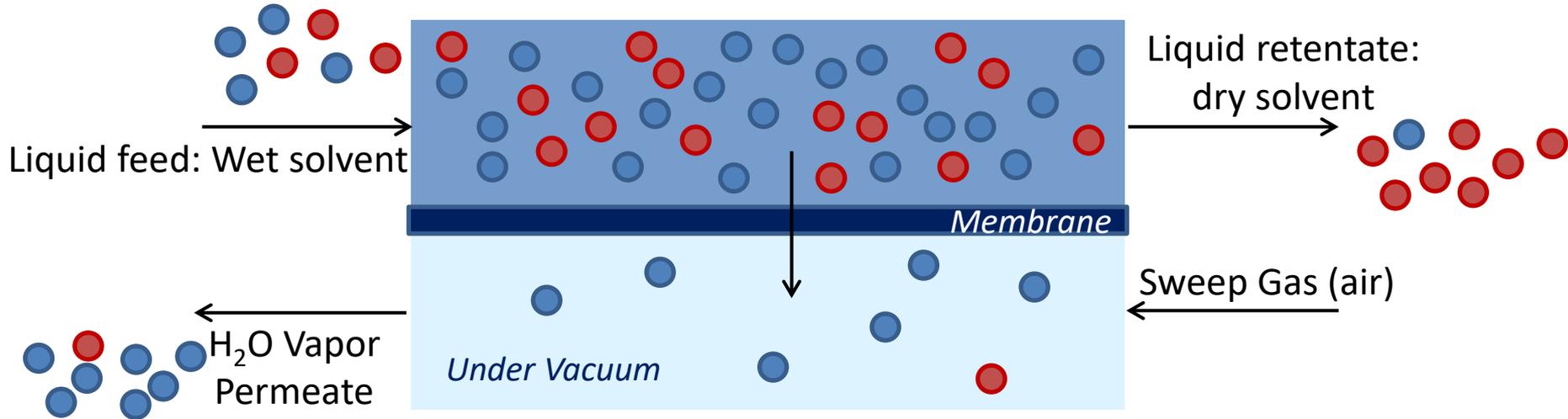
- Specialty chemical
- Semiconductor and electronic manufacturing
- Paint production



Overview of Pervaporation Technology

What is pervaporation?

- Solvent molecule
- Water molecule



$$\text{H}_2\text{O Flux} = \left[\frac{\pi}{\delta} \right] \underbrace{(\gamma \times P^0 - p y)}_{\text{Driving force}}$$

Permeance

- x = water feed mole fraction
- y = water permeate mole fraction
- π = water permeability
- γ = water activity coefficient
- P^0 = water vapor pressure
- δ = membrane thickness
- p = vacuum pressure

What affects driving force?

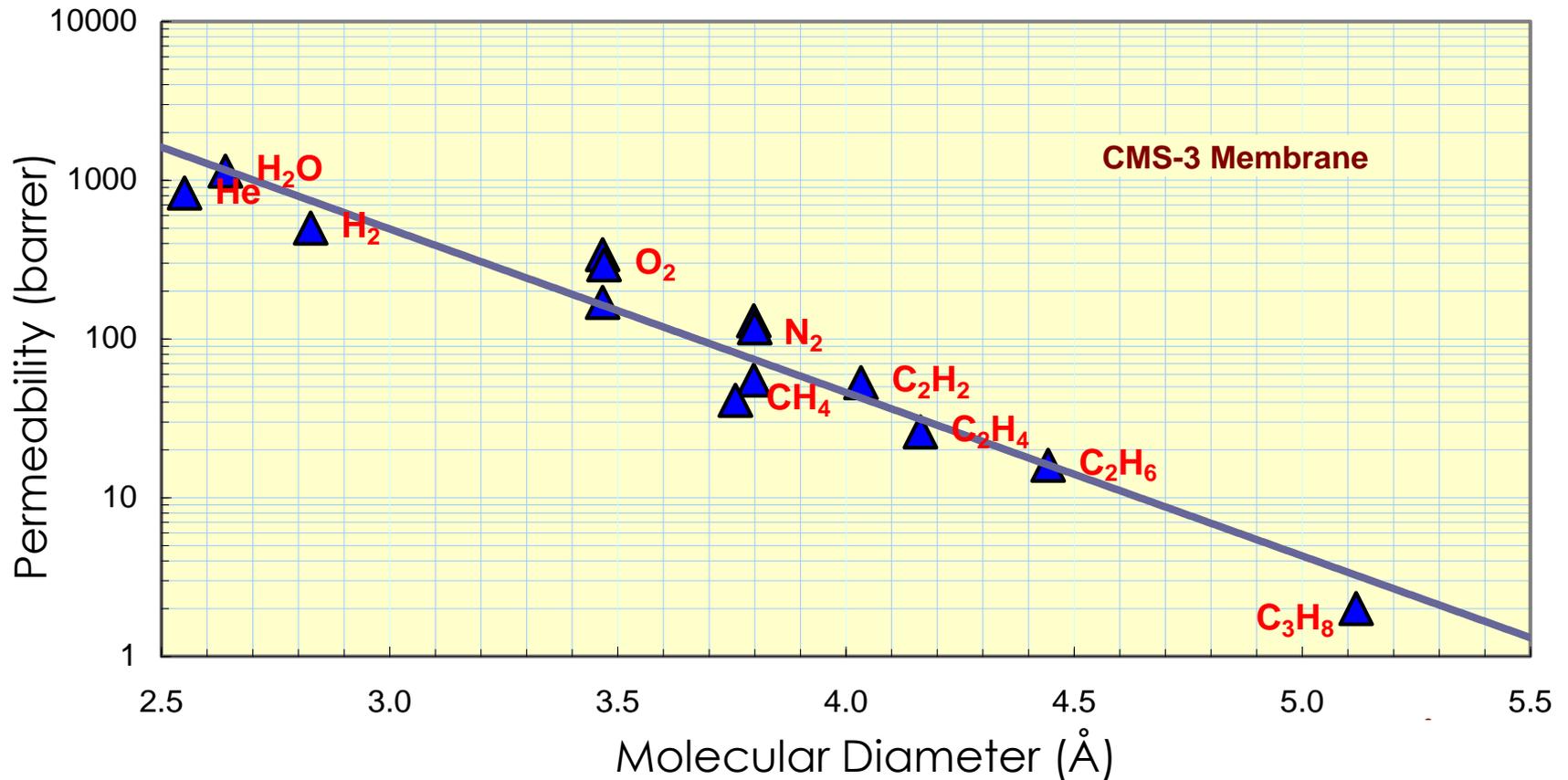
$$\text{H}_2\text{O Flux} = \left[\frac{\pi}{\delta} \right] (\underbrace{\gamma x P^0 - p y}_{\text{Driving force}})$$

Permeance

π = water permeability
 δ = membrane thickness
 γ = water activity coefficient
 x = water feed mole fraction
 P^0 = feed water vapor pressure
 y = water permeate mole fraction
 p = vacuum pressure

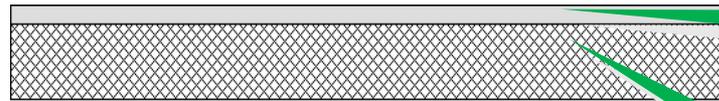
1. **Temperature**: high temperature gives high water vapor pressure
2. **Thermodynamics**: the higher the water activity, the better
3. **Composition**: the higher the water loading, the higher the driving force
4. **Permeate side pressure**: the lower the vacuum, the higher the driving force

What about selectivity?



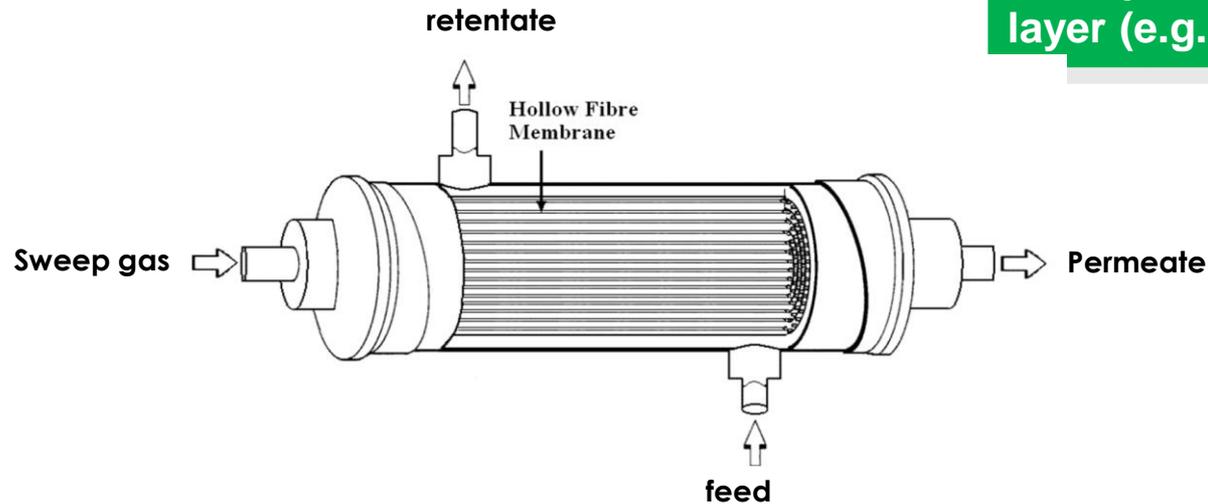
Smaller molecules (e.g., H₂O) go through membrane more quickly

Membrane is a composite structure

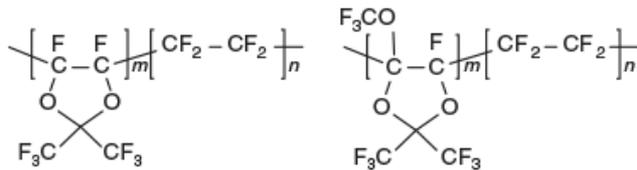
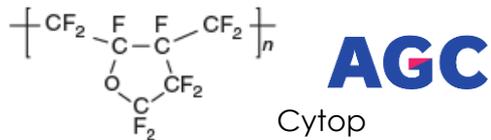


Non-porous
CMS polymer

Microporous support
layer (e.g. ePTFE, PS)



Custom Amorphous Fluouropolymer (CAF) platform



Teflon AF



Hyflon



Amorphous fluouropolymers are known to have high free volume and be chemically resistant

CMS value proposition: Develop custom amorphous fluouropolymers for dehydration of difficult solvents used in manufacturing

- Control separation properties through the introduction of specific monomers to create unique copolymers
- Deep bench of materials - 16 active patents (7 issued)
- Utilize high free volume for high flux and tailor chemistry to allow high selectivity

Important characteristics of pervaporation

- Water goes through membrane, making the system **ideal for removing water from solvent** (NOT removing solvent from water)
- **Azeotropes are not an issue** for pervaporation
- **Separation is not perfect** – there will be some water in the solvent and some solvent in the water
- Can achieve **very high recovery** (>95%)
- **Everything is a tradeoff** – for example, you can get very dry, but you will give up recovery

System design

Considerations for a pervap system

Compatibility

Vacuum level

Solvent mixture

Flow rates

Batch vs. continuous

Pressure drop

Series vs. parallel

Temperature gradients

Membrane longevity

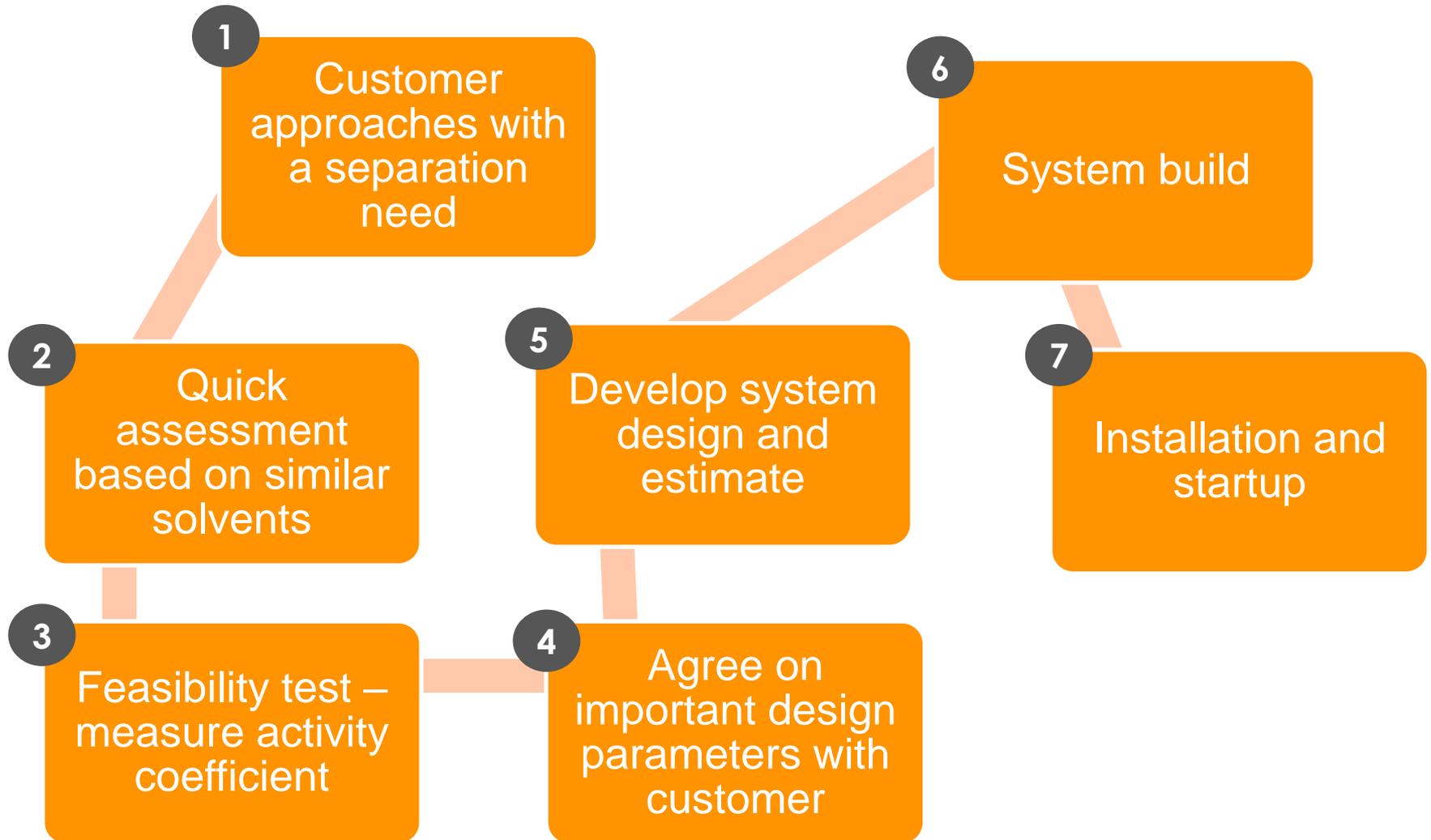
Solvent loss

Recovery vs. purity

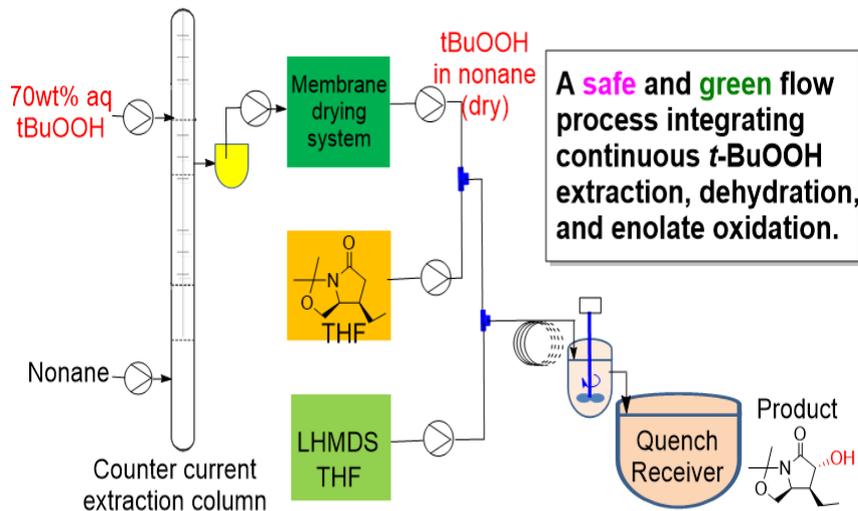
Water level

Impact of salt

Design process overview



Case study: Dehydration of nonane/tert-butyl hydroperoxide (TBHP)



Continuous Production of Anhydrous tert-Butyl Hydroperoxide in Nonane Using Membrane Pervaporation and its Application in Flow Oxidation of a γ -Butyrolactam

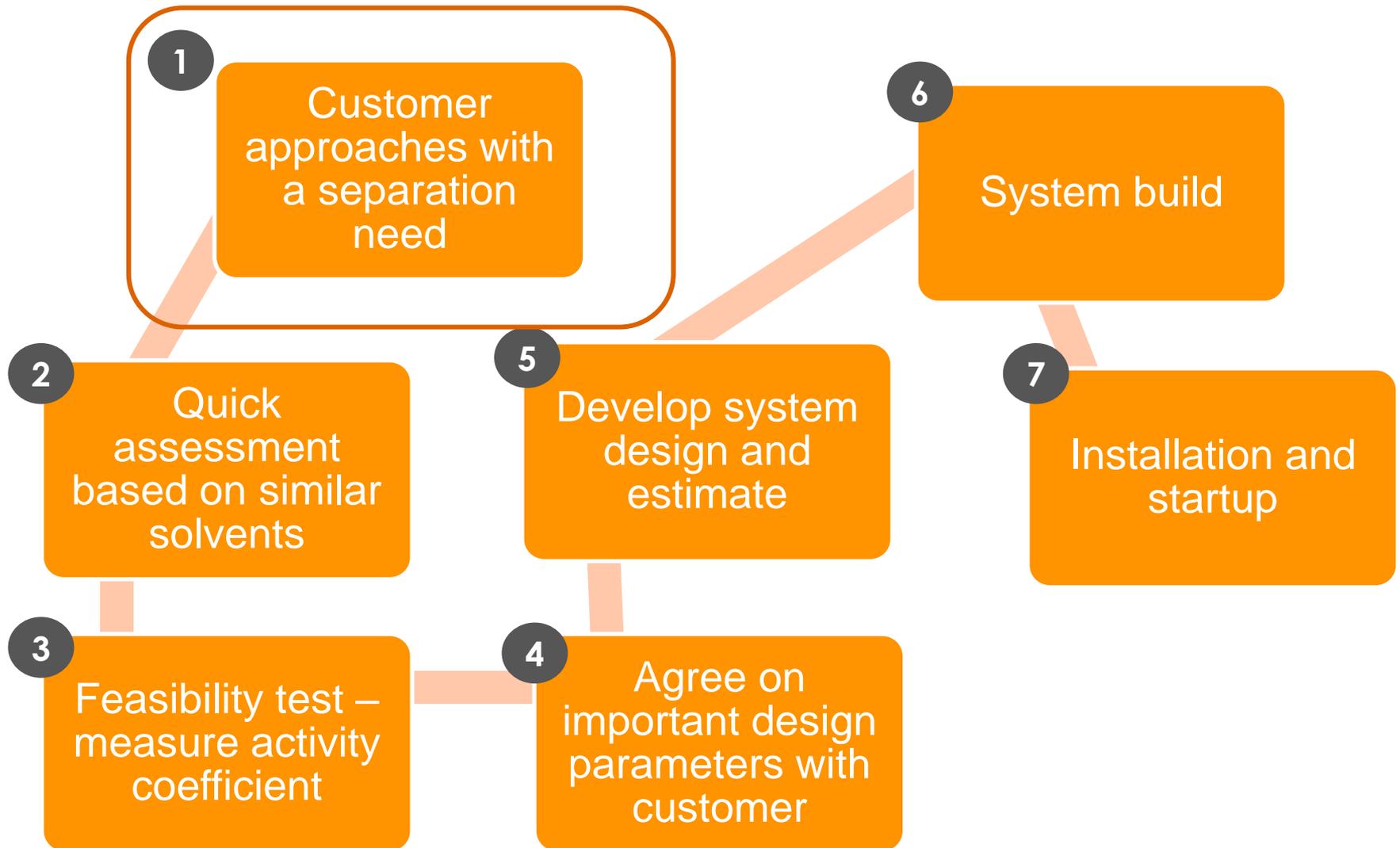
Bryan Li, Steven M. Guinness, Steve Hoagland, Michael W. Fichtner, Hui Kim, Shelly Li, Robert John Maguire, James Christopher McWilliams, Jason Mustakis, Jeffrey Raggon, Dan Campos, Chris Voss, Evan Sohodski, Bryan Feyock, Hannah Murnen, Miguel Gonzalez, Matthew Johnson, Jiangping Lu, Xichun Feng, Xingfang Sun, Songyuan Zheng, and Baolin Wu

Org. Process Res. Dev., Just Accepted Manuscript

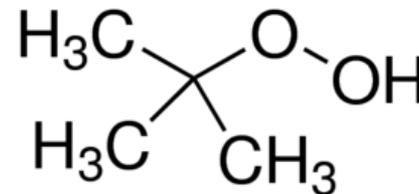
DOI: 10.1021/acs.oprd.8b00083

Publication Date (Web): May 23, 2018

Design process



Objective – Safely use anhydrous TBHP for scaleup of a molecule



- Anhydrous *tert*-butyl hydroperoxide (TBHP) oxidizing agent in many chemical transformations (e.g., Sharpless epoxidation)
- Despite versatility in organic reactions, use of anhydrous TBHP greatly limited due to safety concerns
- Several explosion incidents associated with use of anhydrous TBHP (e.g., overheating during azeotropic distillation)
- Anhydrous TBHP not available on bulk scale – historically avoided for scale up use
- 70 wt% TBHP solution in water is readily available in bulk quantities

Need a method to continuously and safely dehydrate TBHP with minimal holdup volume

1

Customer approaches with a separation need

Questions to ask:

- What is target separation?
- Target purity and recovery?
- What alternative methods have been considered?
- Desired flow rate?
- Batch vs. continuous?
- Temperature constraints?
- Safety concerns?

Design considerations

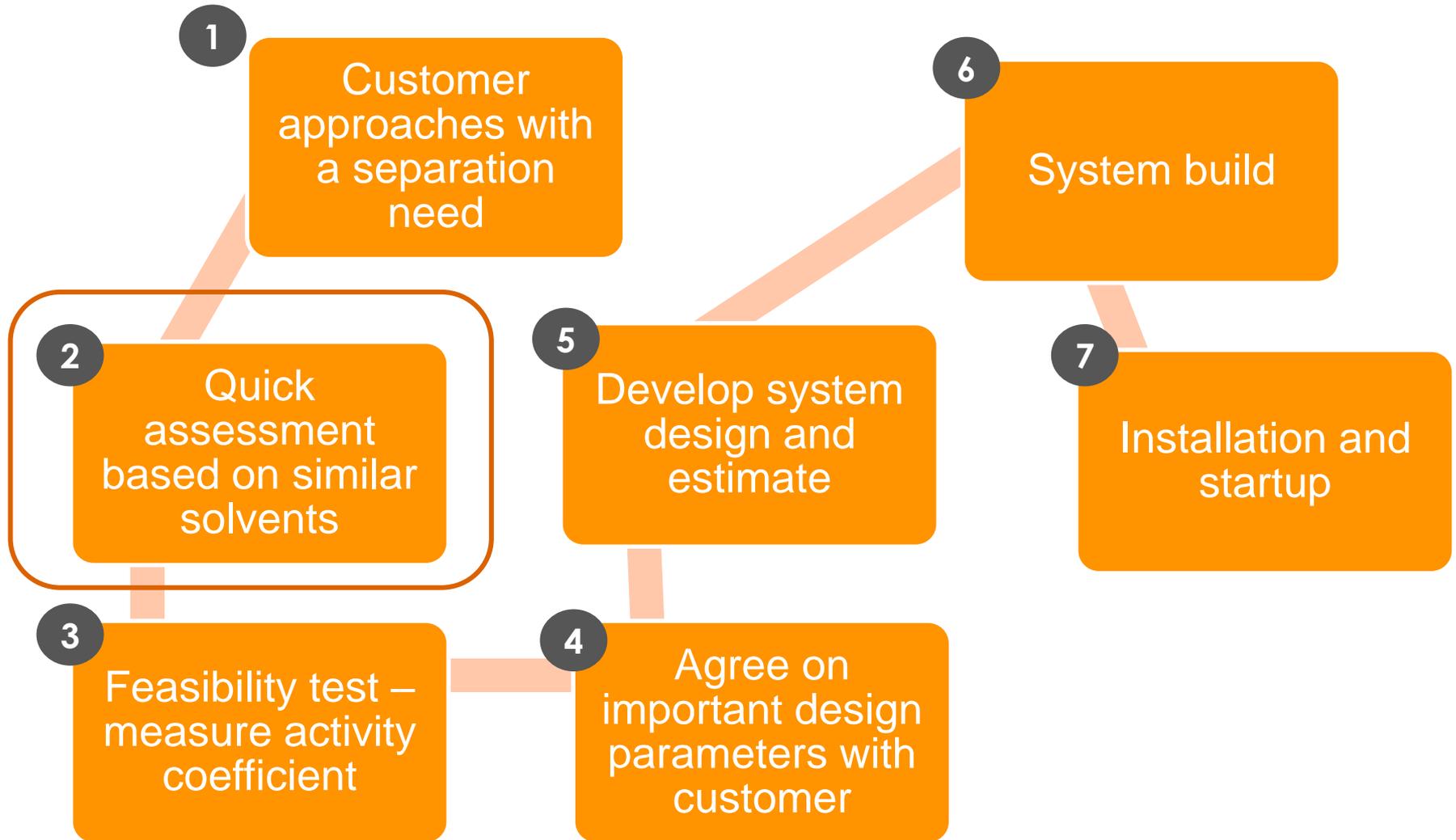
- Compatibility
- Feasibility
- Economics
- Safety

1 Compatible and effective with a variety of solvents

EPA target list of solvents	Effective with CMS technology?
Ethanol	✓
Butanol	✓
Tetrahydrofuran	✓
Dimethylformamide	✓
Methyl isobutyl ketone (MIK)	✓
Acetonitrile	✓ (low recovery)
Methyl tert-butyl ether (MTBE)	✓
Acetone	✓
Isopropanol (IPA)	✓
Methanol	

Additional compatible solvents include: xylene, ethylbenzene, benzene, hexane, cyclohexane, chlorobenzene, ethyl acetate, etc.

Design process

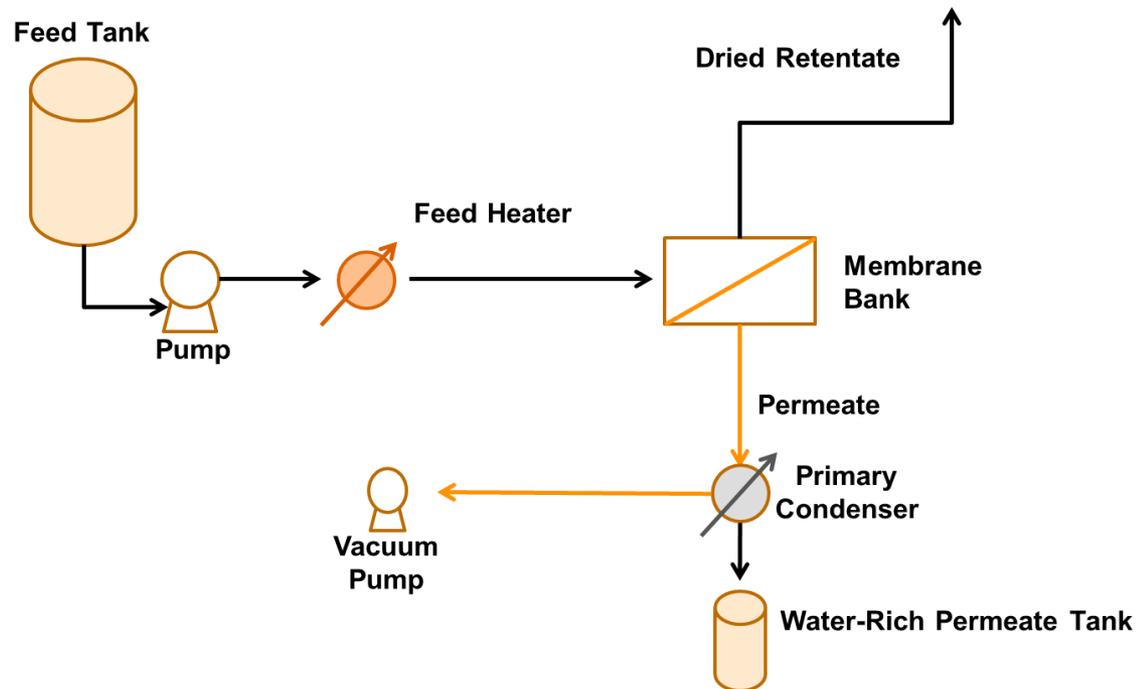


2

Quick assessment based on similar solvents

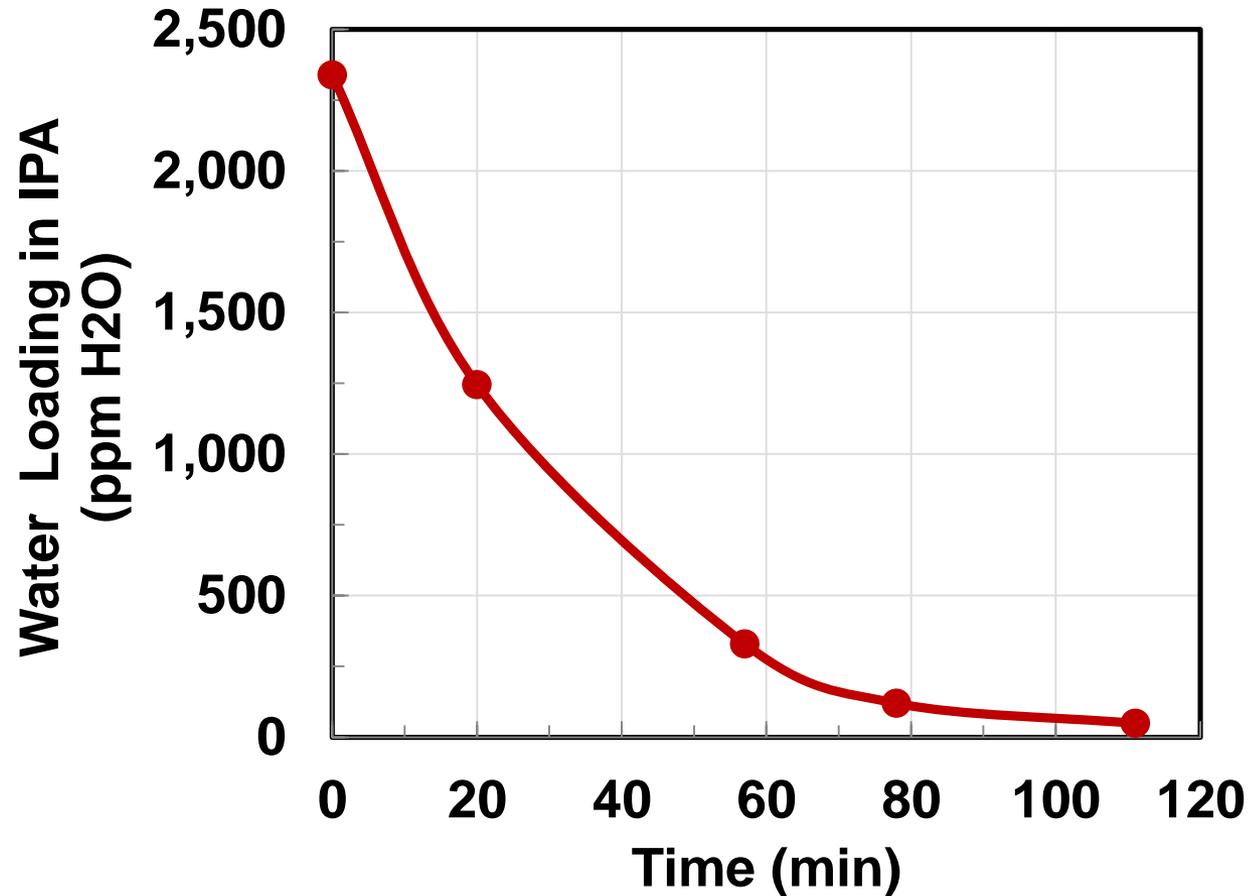
Steps to take

- Use similar solvent to size membrane bank - first order approximation of system cost
- Does that first order approximation meet the economic bar?
- Does it look practical for implementation?

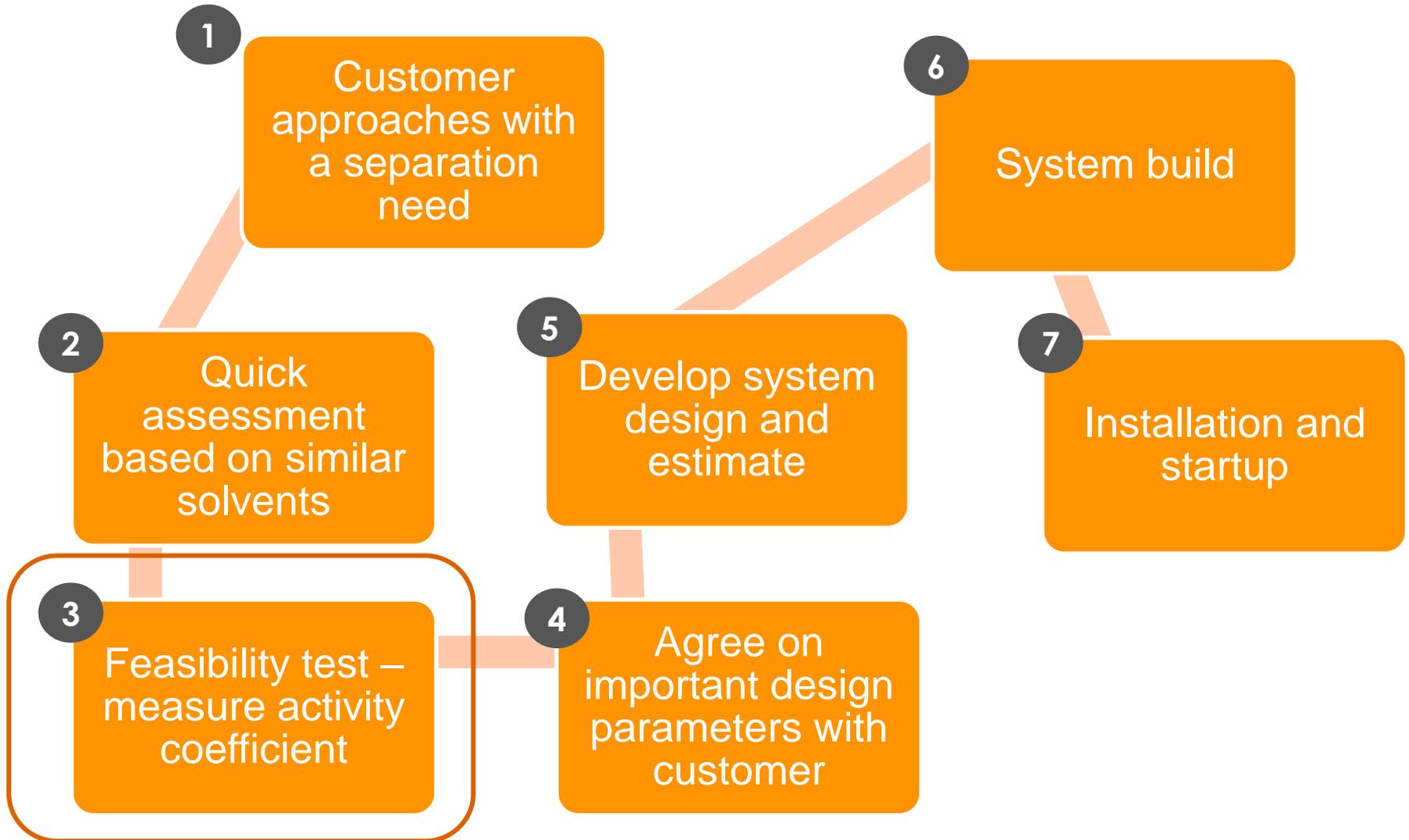


2 Quick assessment based on similar solvents

- Can dry to 99+% solvent as needed
- Works effectively to break water-solvent azeotrope

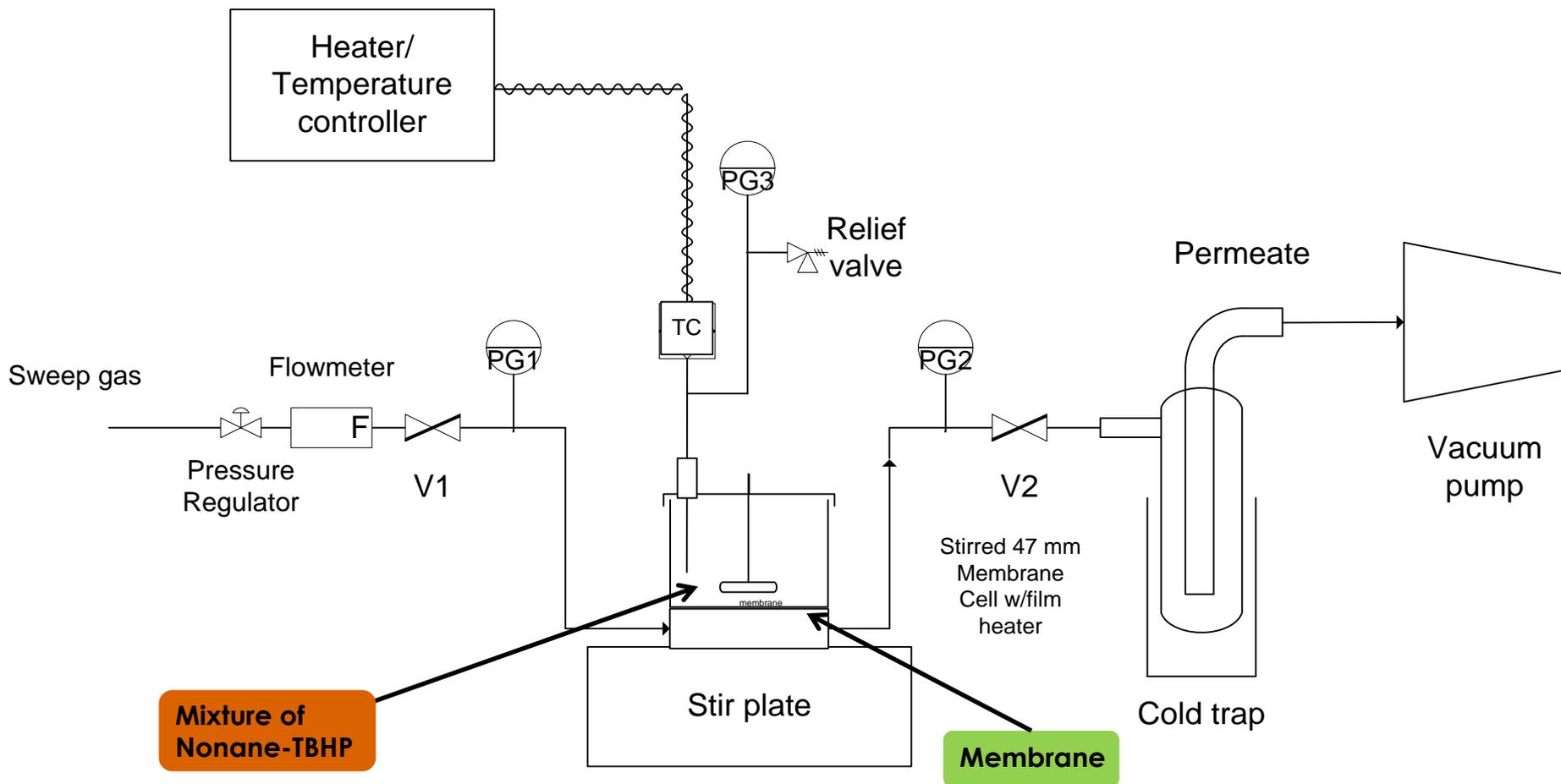


Design process



3

Feasibility test – measure activity coefficient



3

Theoretical pervaporation model used to determine permeability and activity coefficient

$$\ln \frac{x_i}{x_f} = \frac{\pi \gamma A P^o}{m \delta} t$$

Assumptions

- Water partial pressure in permeate ≈ 0
- $m, \pi, \gamma, P^o \approx \text{constant}$

x_i = water initial mole fraction

x_f = water final mole fraction

π = water permeability

γ = water activity coefficient

A = membrane area

P^o = water vapor pressure

m = moles of TBHP solution

δ = membrane thickness

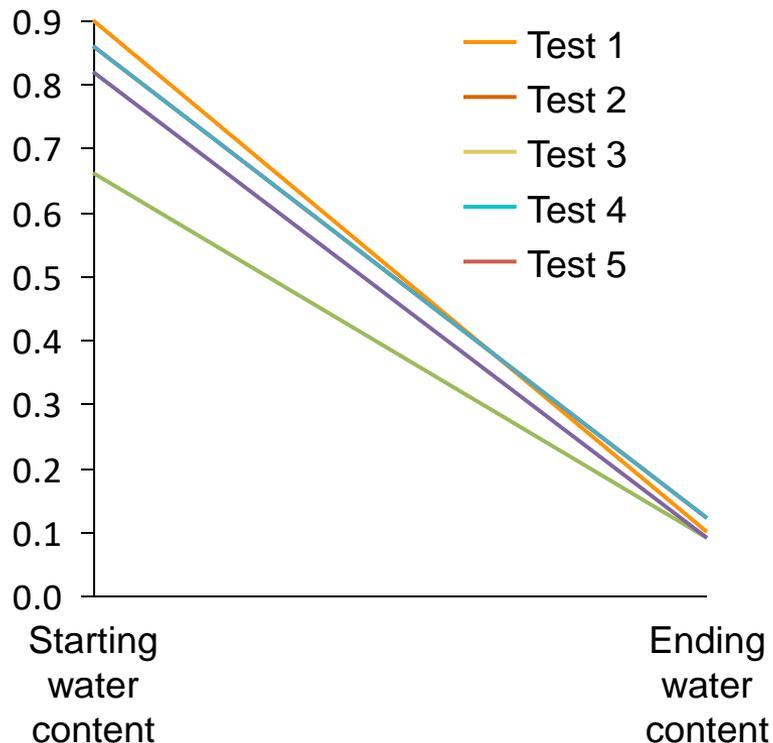
t = time

Once permeability and activity coefficient, membrane area can be determined for full system

3

For all tests, low water content was achieved & water permeability coefficient determined

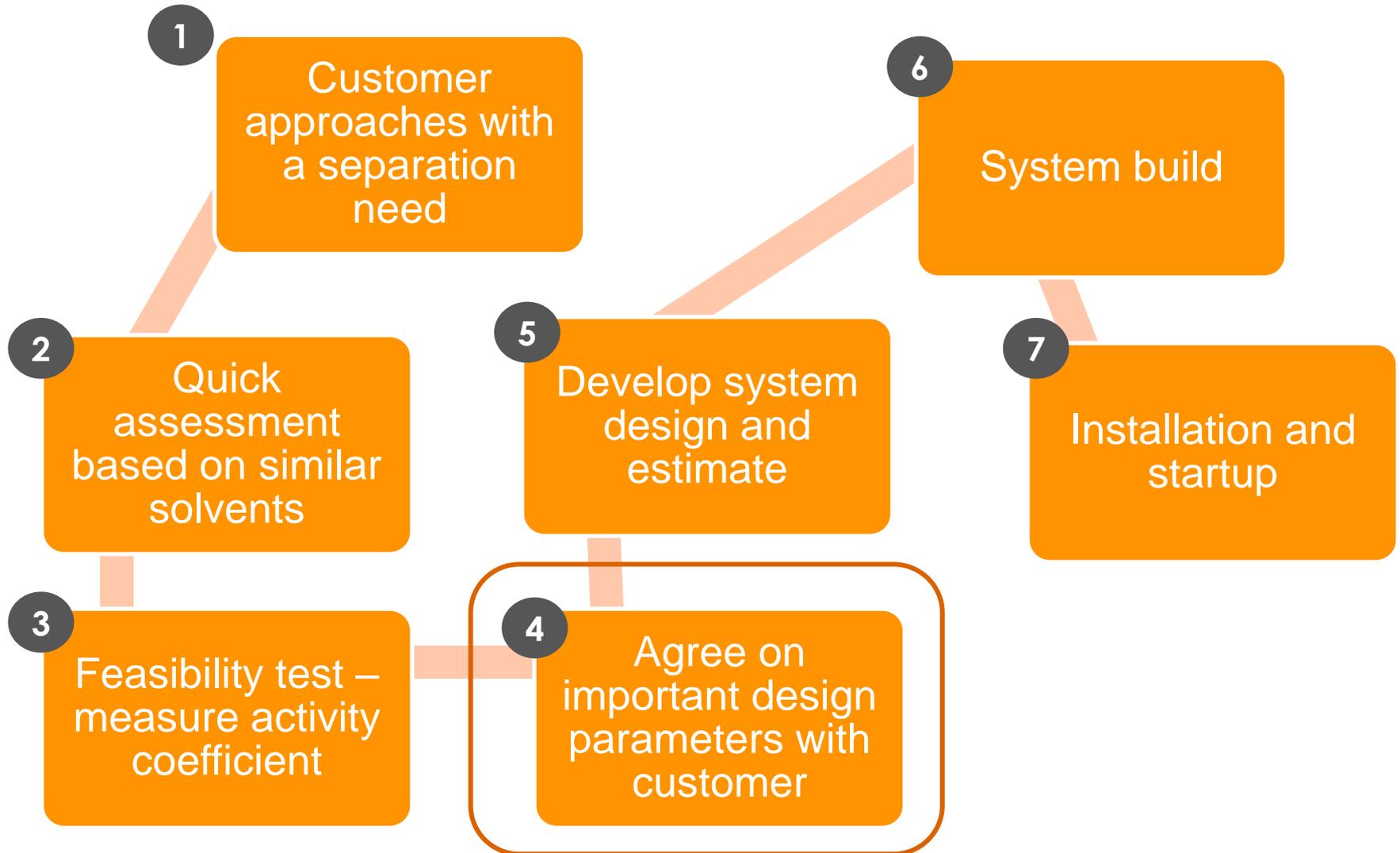
Water content, % wt



Test #	water permeability*activity coefficient		
	(mol- $\mu\text{m}/\text{s}\cdot\text{cm}^2\cdot\text{cmHg}$)	(scc- $\mu\text{m}/\text{s}\cdot\text{cm}^2\cdot\text{cmHg}$)	(Barrer)
1	3.90E-07	0.0087	8728
2	4.03E-07	0.0090	9017
3	3.44E-07	0.0077	7705
4	4.09E-07	0.0091	9147
5	3.92E-07	0.0088	8780
Avg.	3.88E-07	0.0087	8675

Initial mass of TBHP solution=8 g
Sweep rate=100 cc/min

Design process



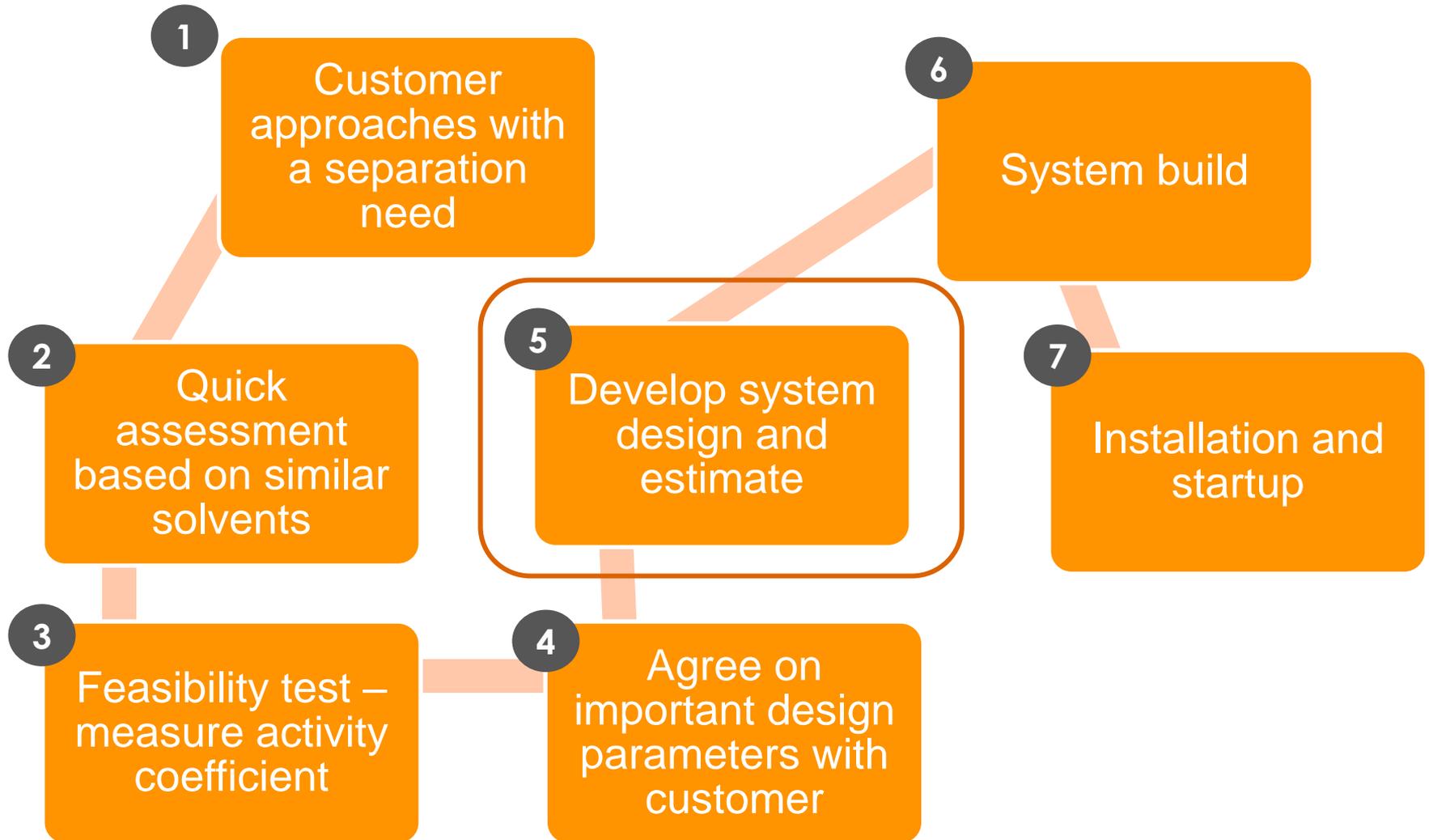
4 Agree on important design parameters with customer

Questions to ask:

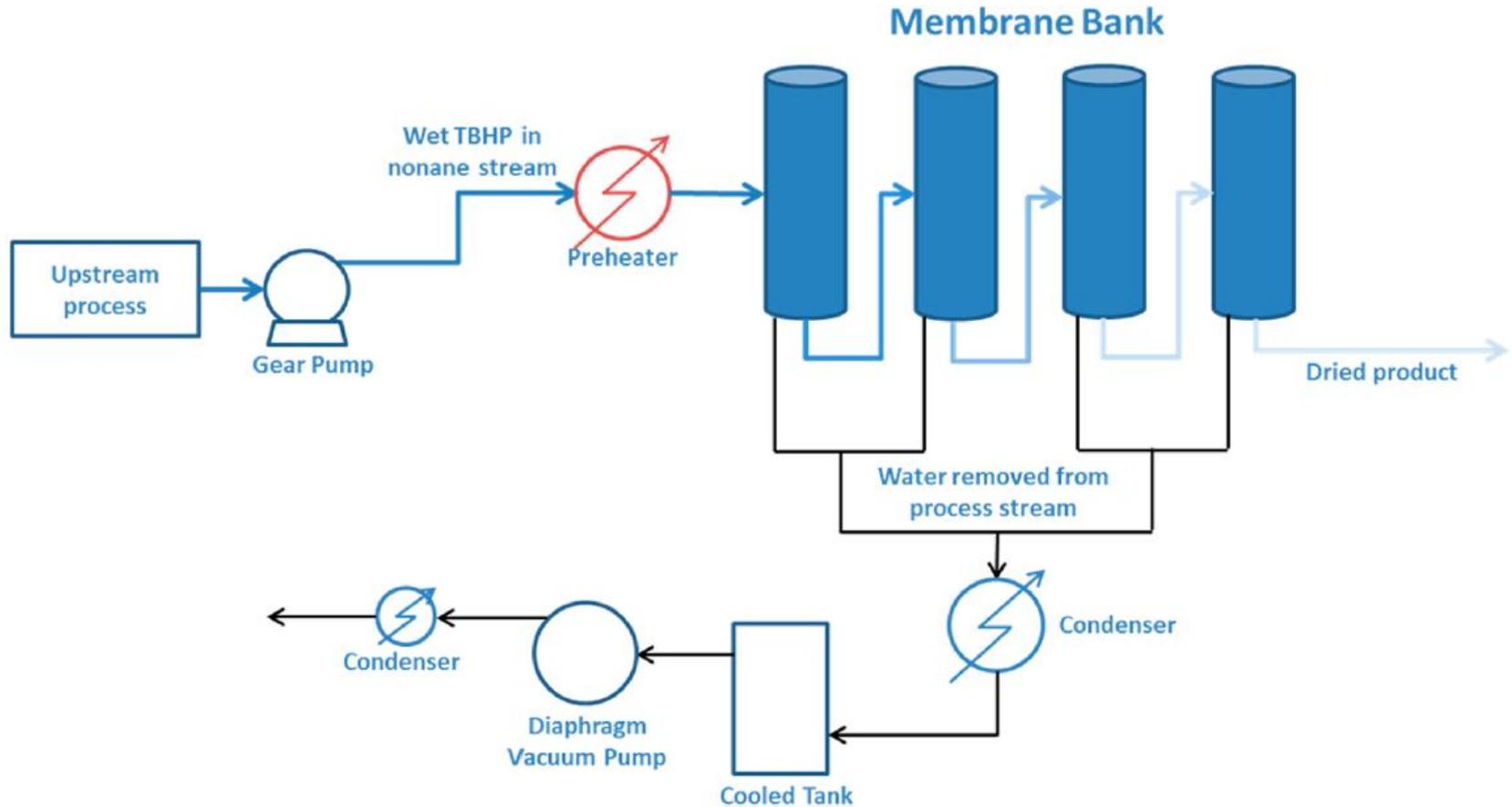
- Flow rates?
- Temperatures
- Safety rating (explosion proof)?
- Holdup volumes
- Controls?
- Integration points?
- Vacuum source?
- Available utilities



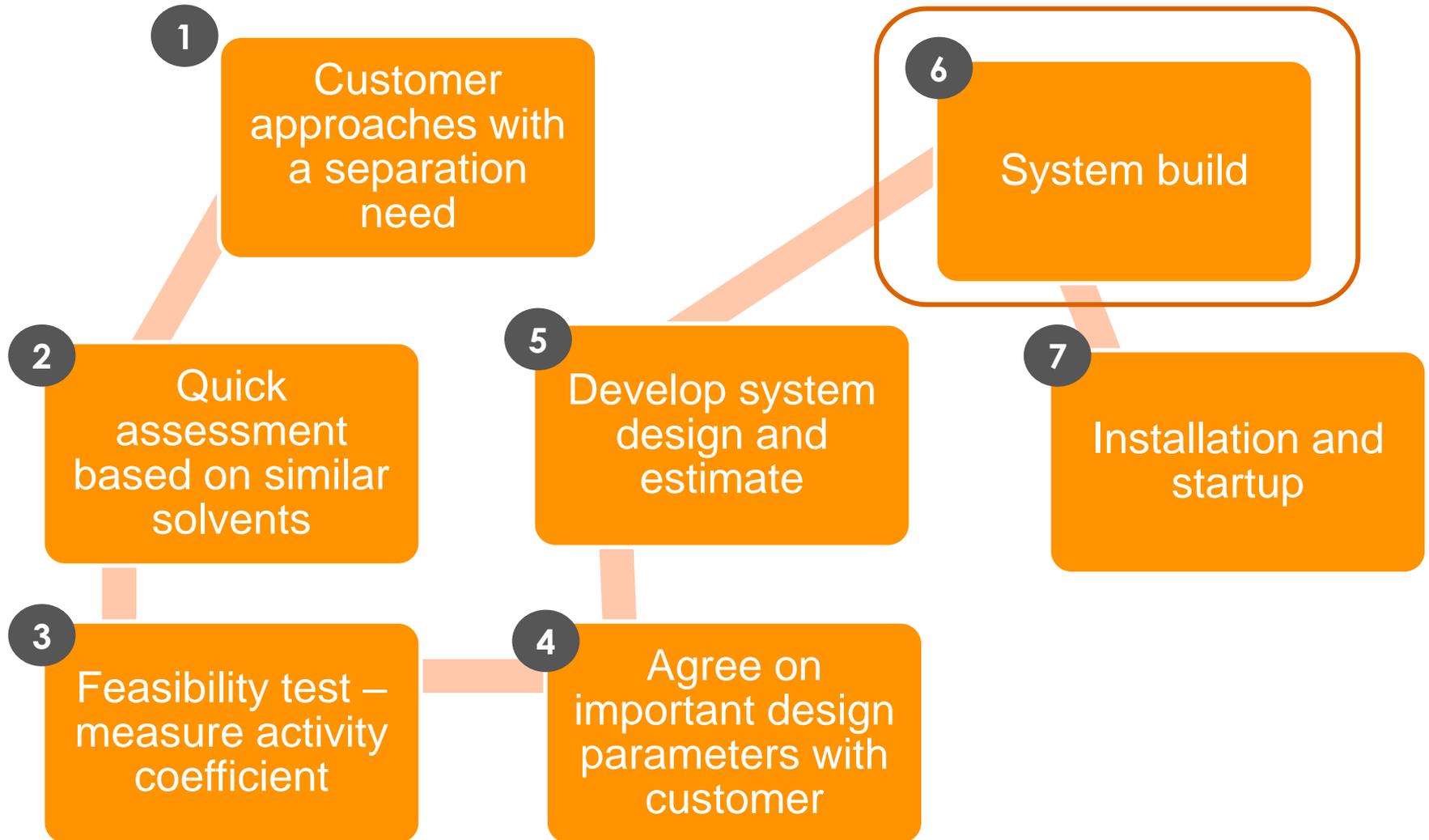
Design process



5 Develop system design and estimate



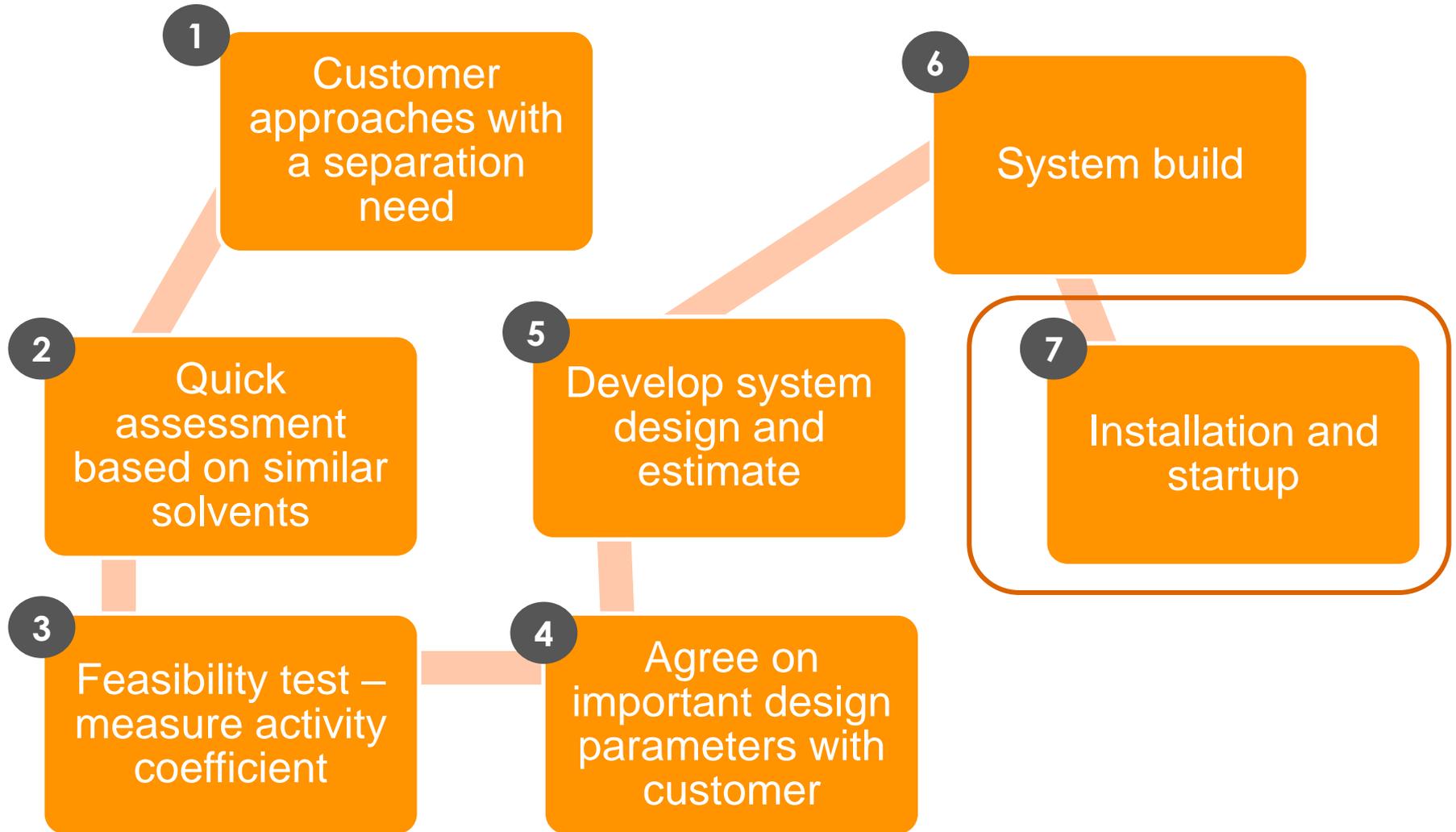
Design process



6 System build



Design process



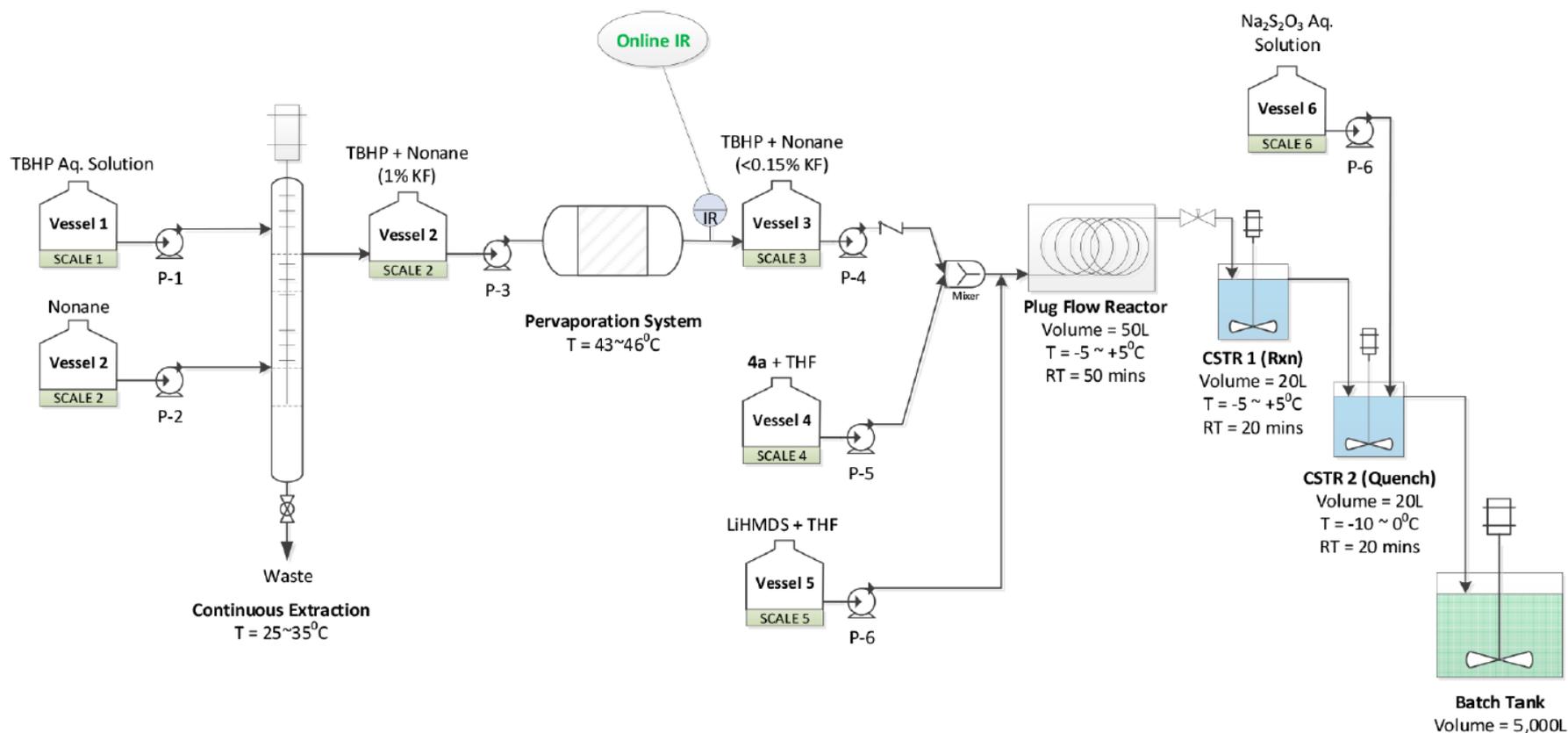
7 Membrane system installed and operational within 3 days



At contract manufacturing site in China

7

Able to run entire reaction using pervaporation system to provide anhydrous TBHP/Nonane



Summary

- Dehydration of solvents is important in the production of pharmaceutical compounds
- Pervaporation using perfluoropolymers is ideal for this unit operation
- A case study has been demonstrated for the dehydration of n-nonane and TBHP

Thank you for your attention

Pfizer

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Asymchem

Miguel Gonzalez
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CMS

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